

THERMODYNAMICS PRACTICE PROBLEMS

1. A Carnot refrigerator has a coefficient of performance of 10. If the refrigerator's interior is to be kept at -45°C , the temperature of the refrigerator's high temperature reservoir is most nearly

- (A) 250K
- (B) 270K
- (C) 300K
- (D) 350K

Solution

For a refrigerator,

$$\text{COP} = \frac{T_{\text{low}}}{T_{\text{high}} - T_{\text{low}}}$$

Solve for the hot side temperature.

$$\begin{aligned} T_{\text{high}} &= \frac{T_{\text{low}}}{\text{COP}} + T_{\text{low}} = \frac{-45^{\circ}\text{C} + 273}{10} + (-45^{\circ}\text{C} + 273) \\ &= 250.8\text{K} \end{aligned}$$

Answer is (A).

2. Helium is compressed isentropically from 1 atmosphere and 5°C to a pressure of 8 atmospheres. The ratio of specific heats for helium is $5/3$. What is the final temperature of the helium?

- (A) 290°C
- (B) 340°C
- (C) 370°C
- (D) 650°C

Solution

$$\frac{T_2}{T_1} = \left(\frac{P_1}{P_2} \right)^{\frac{1-k}{k}}$$

$$\frac{1-k}{k} = \frac{1-\frac{5}{3}}{\frac{5}{3}} = \frac{3-5}{5} = -0.4$$

$$T_2 = T_1 \left(\frac{P_1}{P_2} \right)^{\frac{1-k}{k}} = (5^\circ\text{C} + 273) \left(\frac{1\text{ atm}}{8\text{ atm}} \right)^{-0.4}$$

$$= 638.7\text{K} \quad (366^\circ\text{C})$$

Answer is (C).

3. The thermal efficiency of a Carnot cycle operating between 170°C and 620°C is closest to

- (A) 44%
- (B) 50%
- (C) 63%
- (D) 73%

Solution

$$T_{\text{high}} = 620^\circ\text{C} + 273 = 893\text{K}$$

$$T_{\text{low}} = 170^\circ\text{C} + 273 = 443\text{K}$$

$$\eta_{\text{Carnot}} = \frac{T_{\text{high}} - T_{\text{low}}}{T_{\text{high}}} = \frac{893\text{K} - 443\text{K}}{893\text{K}} = 0.504 \quad (50.4\%)$$

Answer is (B).

4. Superheated steam at 4.0 MPa and 275°C expands isentropically to 1.4 MPa. What is the quality factor of the resulting vapor? The data for the steam are as follows.

For 4.0 MPa, 275°C:	$h = 2886.2\text{ kJ/kg}$; $s = 6.2285\text{ kJ/kg} \cdot \text{K}$
For 1.4 MPa, dry saturated vapor:	$h_g = 2790.0\text{ kJ/kg}$; $s_g = 6.4693\text{ kJ/kg} \cdot \text{K}$
For 1.4 MPa, saturated liquid:	$h_f = 830.3\text{ kJ/kg}$; $s_f = 2.2842\text{ kJ/kg} \cdot \text{K}$

- (A) 91%
- (B) 92%
- (C) 93%
- (D) 94%

Solution

The entropy is unchanged in an isentropic process.

$$s = xs_g + (1-x)s_f$$

$$6.2285 \frac{\text{kJ}}{\text{kg} \cdot \text{K}} = x \left(6.4693 \frac{\text{kJ}}{\text{kg} \cdot \text{K}} \right) + (1-x) \left(2.2842 \frac{\text{kJ}}{\text{kg} \cdot \text{K}} \right)$$

$$4.1851x = 3.9443$$

$$x = 0.9425$$

Answer is (D).

5. A compressor takes atmospheric air (molecular weight of 29 kg/kmol) at 103.4 kPa and 20°C and delivers it at 1.034 MPa and 175°C. The compression process is polytropic. The work required to compress one unit mass of air is most nearly

- (A) 50 kJ/kg
- (B) 100 kJ/kg
- (C) 150 kJ/kg
- (D) 200 kJ/kg

Solution

For a process with polytropic exponent n ,

$$\frac{T_1}{T_2} = \left(\frac{P_1}{P_2} \right)^{\frac{n-1}{n}}$$

$$\frac{20^\circ\text{C} + 273}{175^\circ\text{C} + 273} = \left(\frac{103.4 \text{ kPa}}{1034 \text{ kPa}} \right)^{\frac{n-1}{n}}$$

$$0.6540 = (0.10)^{\frac{n-1}{n}}$$

Take the base-10 logarithm of both sides.

$$\log(0.6540) = \left(\frac{n-1}{n} \right) \log(0.10)$$

$$\frac{n-1}{n} = 0.1844$$

$$n = 1.23$$

If air's specific gas constant is not known, it can be calculated.

$$R = \frac{\bar{R}}{\text{molecular weight}} = \frac{8.314 \frac{\text{kJ}}{\text{kmol} \cdot \text{K}}}{29 \frac{\text{kg}}{\text{kmol}}} = 0.2867 \text{ kJ/kg} \cdot \text{K}$$

$$w = \frac{P_2 v_2 - P_1 v_1}{1 - n} = \frac{R(T_2 - T_1)}{1 - n}$$

$$= \frac{\left(0.2867 \frac{\text{kJ}}{\text{kg} \cdot \text{K}}\right)(175^\circ\text{C} - 20^\circ\text{C})}{1 - 1.23} = -193.2 \text{ kJ/kg}$$

Answer is (D).

6. When 1.5 kg of an ideal gas (specific heat at constant volume = 0.8216 kJ/kg×K) is heated at constant volume to a final temperature of 425°C, the total entropy increase is 0.4386 kJ/K. The initial temperature of the gas is most nearly

- (A) 200°C
- (B) 210°C
- (C) 220°C
- (D) 240°C

Solution

The total entropy increase for an ideal gas is

$$\Delta S = m \left(c_v \ln \left(\frac{T_2}{T_1} \right) + R \ln \left(\frac{v_2}{v_1} \right) \right)$$

$$v_2 = v_1$$

$$0.4386 \frac{\text{kJ}}{\text{K}} = (1.5 \text{ kg}) \left(\left(0.8216 \frac{\text{kJ}}{\text{kg} \cdot \text{K}} \right) \ln \left(\frac{425^\circ\text{C} + 273}{T_1} \right) \right)$$

$$\ln \left(\frac{698 \text{ K}}{T_1} \right) = 0.3559$$

Take the antilogarithm of both sides and solve for T_1 .

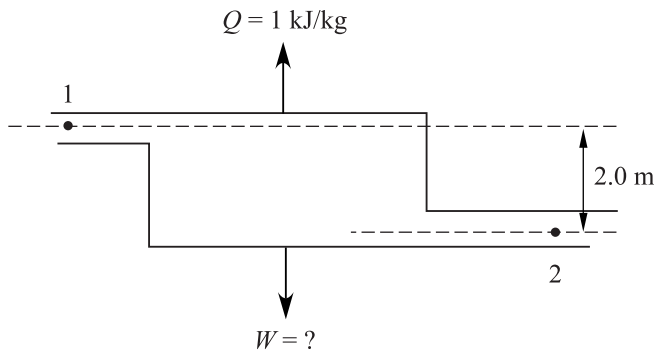
$$T_1 = 489\text{K} \quad (489\text{K} - 273 = 216^\circ\text{C})$$

Answer is (C).

7. Steam enters a turbine with a velocity of 40 m/s and an enthalpy of 3433.8 kJ/kg. At the outlet, 2 meters lower than the inlet, the velocity is 162 m/s, and the enthalpy is 2675.5 kJ/kg. A heat loss of 1 kJ/kg is experienced from the turbine casing. The work output per unit mass is closest to

- (A) 650 kJ/kg
- (B) 700 kJ/kg
- (C) 720 kJ/kg
- (D) 750 kJ/kg

Solution



The steady flow energy equation is

$$\begin{aligned} \dot{W}_{\text{out}} &= \dot{m} \left[\left(h_{\text{in}} + \frac{V_{\text{in}}^2}{2} + Z_{\text{in}}g \right) - \left(h_{\text{exit}} + \frac{V_{\text{exit}}^2}{2} + Z_{\text{exit}}g \right) \right] + \dot{Q}_{\text{in}} \\ \frac{\dot{W}_{\text{out}}}{\dot{m}} &= \left(3433.8 \frac{\text{kJ}}{\text{kg}} + \frac{\left(40 \frac{\text{m}}{\text{s}} \right)^2}{(2) \left(1000 \frac{\text{J}}{\text{kJ}} \right)} + \frac{(2 \text{ m}) \left(9.81 \frac{\text{m}}{\text{s}^2} \right)}{1000 \frac{\text{J}}{\text{kJ}}} \right) \\ &\quad - \left(2675.5 \frac{\text{kJ}}{\text{kg}} + \frac{\left(162 \frac{\text{m}}{\text{s}} \right)^2}{(2) \left(1000 \frac{\text{J}}{\text{kJ}} \right)} + 0 \right) - 1 \frac{\text{kJ}}{\text{kg}} \\ &= 744.9 \text{ kJ/kg} \end{aligned}$$

Answer is (D).

8. Compressed carbon dioxide (molecular weight = 44) is kept in a full 0.5 m³ tank at 100°C and 500 kPa. The mass of the carbon dioxide in the tank is most nearly

- (A) 3.0 kg
- (B) 3.3 kg
- (C) 3.5 kg
- (D) 4.1 kg

Solution

The specific gas constant is

$$R = \frac{\bar{R}}{\text{molecular weight}} = \frac{8.314 \frac{\text{kJ}}{\text{kmol} \cdot \text{K}}}{44 \frac{\text{kg}}{\text{kmol}}} = 0.1890 \text{ kJ/kg} \cdot \text{K}$$

Use the ideal gas law.

$$PV = mRT$$
$$m = \frac{pV}{RT} = \frac{(500 \text{ kPa})(0.5 \text{ m}^3)}{\left(0.1890 \frac{\text{kJ}}{\text{kg} \cdot \text{K}}\right)(100^\circ\text{C} + 273)}$$

Answer is (C).

9. A Carnot refrigeration cycle is used to keep a freezer at -5°C. Heat is rejected at 20°C. If the heat removal rate is 30 kW, the COP of the refrigeration cycle is most nearly

- (A) 9
- (B) 10
- (C) 11
- (D) 12

Solution

$$T_{\text{high}} = 20^\circ\text{C} + 273 = 293\text{K}$$

$$T_{\text{low}} = -5^\circ\text{C} + 273 = 268\text{K}$$

$$\text{COP} = \frac{T_{\text{low}}}{T_{\text{high}} - T_{\text{low}}} = \frac{268\text{K}}{293\text{K} - 268\text{K}} = 10.7$$

Answer is (C).

10. 0.2 kg of air is heated in a constant volume process from 20°C to 100°C. The specific heat at constant volume is 0.7186 kJ/kg · K . The change in entropy for the heating process is most nearly

- (A) 0.028 kJ/K
- (B) 0.033 kJ/K
- (C) 0.035 kJ/K
- (D) 0.039 kJ/K

Solution

$$\Delta S = m \left(c_v \ln \left(\frac{T_2}{T_1} \right) + R \ln \left(\frac{v_2}{v_1} \right) \right)$$

$$v_2 = v_1$$

$$\begin{aligned} \Delta S &= 0.2 \text{ kg} \left(0.7186 \frac{\text{kJ}}{\text{kg} \cdot \text{K}} \right) \ln \left(\frac{100^\circ\text{C} + 273}{20^\circ\text{C} + 273} \right) \\ &= 0.0347 \end{aligned}$$

Answer is (C).