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## Problems

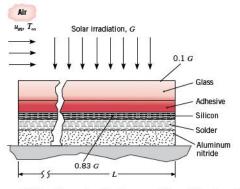
 $5 \times 10^5$ , for what values of  $Re_L$  would the total heat transfer be independent of orientation?

- 7.14 In fuel cell stacks, it is desirable to operate under conditions that promote uniform surface temperatures for the electrolytic membranes. This is especially true in high-temperature fuel cells where the membrane is constructed of a brittle ceramic material. Electrochemical reactions in the electrolytic membranes generate thermal energy, while gases flowing above and below the membranes cool it. The stack designer may specify top and bottom flows that are in the same, opposite, or orthogonal directions. A preliminary study of the effect of the relative flow directions is conducted whereby a 150 mm × 150 mm thin sheet of material, producing a uniform heat flux of 100 W/m<sup>2</sup>, is cooled (top and bottom) by air with a free stream temperature and velocity of 25°C and 2 m/s, respectively.
  - (a) Determine the minimum and maximum local membrane temperatures for top and bottom flows that are in the same, opposite, and orthogonal directions. Which flow configuration minimizes the membrane temperature? *Hint*: For the opposite and orthogonal flow cases, the boundary layers are subject to boundary conditions that are neither uniform temperature nor uniform heat flux. It is, however, reasonable to expect that the resulting temperatures would be *bracketed* by your answers based on the constant heat flux and constant temperature boundary conditions.
  - (b) Plot the surface temperature distribution T(x) for the cases involving flow in the opposite and same directions. Thermal stresses are undesirable and are related to the spatial temperature gradient along the membrane. Which configuration minimizes spatial temperature gradients?
- 7.15 Air at a pressure of 1 atm and a temperature of 50°C is in parallel flow over the top surface of a flat plate that is heated to a uniform temperature of 100°C. The plate has a length of 0.20 m (in the flow direction) and a width of 0.10 m. The Reynolds number based on the plate length is 40,000. What is the rate of heat transfer from the plate to the air? If the free stream velocity of the air is doubled and the pressure is increased to 10 atm, what is the rate of heat transfer?
- 7.16 Consider a rectangular fin that is used to cool a motorcycle engine. The fin is 0.15 m long and at a temperature of 250°C, while the motorcycle is moving at 80 km/h in air at 27°C. The air is in parallel flow over both surfaces of the fin, and turbulent flow conditions may be assumed to exist throughout.
  - (a) What is the rate of heat removal per unit width of the fin?

(b) Generate a plot of the heat removal rate per unit width of the fin for motorcycle speeds ranging from 10 to 100 km/h.

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- 7.17 The Weather channel reports that it is a hot, muggy day with an air temperature of 90°F, a 10 mph breeze out of the southwest, and bright sunshine with a solar insolation of 400 W/m<sup>2</sup>. Consider the wall of a metal building over which the prevailing wind blows. The length of the wall in the wind direction is 10 m, and the emissivity is 0.93. Assume that all the solar irradiation is absorbed, that irradiation from the sky is negligible, and that flow is fully turbulent over the wall. Estimate the average wall temperature.
- **7.18** A photovoltaic solar panel consists of a sandwich of (top to bottom) a 3-mm-thick ceria-doped glass ( $k_g = 1.4 \text{ W/m} \cdot \text{K}$ ), a 0.1-mm-thick optical grade adhesive ( $k_a = 145 \text{ W/m} \cdot \text{K}$ ), a very thin silicon semiconducting material, a 0.1-mm-thick solder layer ( $k_s = 50 \text{ W/m} \cdot \text{K}$ ) and a 2-mm-thick solder layer ( $k_s = 50 \text{ W/m} \cdot \text{K}$ ) and a 2-mm-thick solder layer ( $k_s = 120 \text{ W/m} \cdot \text{K}$ ). The solar-to-electrical conversion efficiency within the semiconductor depends on the silicon temperature,  $T_{si}$ , and is described by the expression  $\eta = 0.28 0.001T_{sip}$  where  $T_{si}$  is in °C, for  $25^{\circ}\text{C} \leq T_{si} \leq 250^{\circ}\text{C}$ . Ten percent of the solar irradiation is absorbed at the top surface of the glass, while 83% of the solar irradiation is transmitted to and absorbed by the silicon (the remaining 7% is reflected away from the cell). The glass has an emissivity of 0.90.



(a) Consider an L = 1 m long, w = 0.1 m wide solar cell that is placed on an insulated surface. Determine the silicon temperature and the electric power produced by the solar cell for an air velocity of 4 m/s parallel to the long direction, with air and surroundings temperatures of 25°C. The solar irradiation is 700 W/m<sup>2</sup>. The boundary layer is tripped to a turbulent condition at the leading edge of the panel. User name: Constantine Tarawneh Book: Fundamentals of Heat and Mass Transfer, 6th Edition Page: 468. No part of any book may be reproduced or transmitted by any means without the publisher's prior permission. Use (other than qualified fair use) in violation of the law or Terms of Service is prohibited. Violators will be prosecuted to the full extent of the law.

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Chapter 7 External Flow

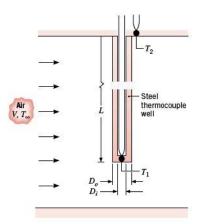
2024 aluminum pin fin through the wall separating the two fluids. The pin is inserted to a depth of d into fluid 1. Fluid 1 is air with a mean temperature of 10°C and nearly uniform velocity of 10 m/s. Fluid 2 is air with a mean temperature of 40°C and mean velocity of 3 m/s.

- (a) Determine the rate of heat transfer from the warm air to the cool air through the pin fin for d = 50 mm.
- (b) Plot the variation of the heat transfer rate with the insertion distance, *d*. Does an optimal insertion distance exist?
- 7.55 Repeat Problem 7.54, except now fluid 1 is ethylene glycol with a mean temperature of 10°C and nearly uniform velocity of 10 m/s. Fluid 2 is water with a mean temperature of 40°C and mean velocity of 3 m/s.
- 7.56 Hot water at 50°C is routed from one building in which it is generated to an adjoining building in which it is used for space heating. Transfer between the buildings occurs in a steel pipe (k = 60 W/m ⋅ K) of 100-mm outside diameter and 8-mm wall thickness. During the winter, representative environmental conditions involve air at T<sub>∞</sub> = -5°C and V = 3 m/s in cross flow over the pipe.
  - (a) If the cost of producing the hot water is \$0.05 per kW · h, what is the representative daily cost of heat loss from an uninsulated pipe to the air per meter of pipe length? The convection resistance associated with water flow in the pipe may be neglected.
  - (b) Determine the savings associated with application of a 10-mm-thick coating of urethane insulation (k = 0.026 W/m · K) to the outer surface of the pipe.
- 7.57 An uninsulated steam pipe is used to transport high-temperature steam from one building to another. The pipe is of 0.5-m diameter, has a surface temperature of 150°C, and is exposed to ambient air at -10°C. The air moves in cross flow over the pipe with a velocity of 5 m/s.

(a) What is the heat loss per unit length of pipe?

- (b) Consider the effect of insulating the pipe with a rigid urethane foam (k = 0.026 W/m · K). Evaluate and plot the heat loss as a function of the thickness  $\delta$  of the insulation layer for  $0 \le \delta \le 50$  mm.
- **7.58** A thermocouple is inserted into a hot air duct to measure the air temperature. The thermocouple  $(T_1)$  is soldered to the tip of a steel *thermocouple well* of length L = 0.15 m and inner and outer diameters of  $D_i = 5$  mm and  $D_o = 10$  mm. A second thermocouple  $(T_2)$  is used to measure the duct wall temperature.

Consider conditions for which the air velocity in the duct is V = 3 m/s and the two thermocouples register temperatures of  $T_1 = 450$  K and  $T_2 = 375$  K. Neglecting radiation, determine the air temperature  $T_{\infty}$ . Assume that,



for steel,  $k = 35 \text{ W/m} \cdot \text{K}$ , and, for air,  $\rho = 0.774 \text{ kg/m}^3$ ,  $\mu = 251 \times 10^{-7} \text{ N} \cdot \text{s/m}^2$ ,  $k = 0.0373 \text{ W/m} \cdot \text{K}$ , and Pr = 0.686.

- **7.59** Consider conditions for which a mercury-in-glass thermometer of 4-mm diameter is inserted to a length *L* through the wall of a duct in which air at 77°C is flowing. If the stem of the thermometer at the duct wall is at the wall temperature  $T_w = 15^{\circ}$ C, conduction heat transfer through the glass causes the bulb temperature to be lower than that of the airstream.
  - (a) Develop a relationship for the *immersion* error, ΔT<sub>i</sub> = T(L) - T<sub>∞</sub>, as a function of air velocity, thermometer diameter, and insertion length L.
  - (b) To what length L must the thermometer be inserted if the immersion error is not to exceed 0.25°C when the air velocity is 10 m/s?
  - (c) Using the insertion length determined in part (b), calculate and plot the immersion error as a function of air velocity for the range 2 to 20 m/s.
  - (d) For a given insertion length, will the immersion error increase or decrease if the diameter of the thermometer is increased? Is the immersion error more sensitive to the diameter or air velocity?
- 7.60 Fluid velocities can be measured using hot-film sensors, and a common design is one for which the sensing element forms a thin film about the circumference of a quartz rod. The film is typically comprised of a thin (~100 nm) layer of platinum, whose electrical resistance is proportional to its temperature. Hence, when submerged in a fluid stream, an electric current may be passed through the film to maintain its temperature above that of the fluid. The temperature of the film is

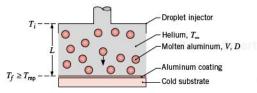
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## Chapter 7 External Flow

K, estimate the time-in-flight required to heat a particle to its melting point,  $T_{mp}$ , and, once at  $T_{mp}$ , for the particle to experience complete melting. Is the prescribed value of L sufficient to ensure complete particle melting before surface impact?

7.76 Highly reflective aluminum coatings may be formed on the surface of a substrate by impacting the surface with molten drops of aluminum. The droplets are discharged from an injector, proceed through an inert gas (helium), and must still be in a molten state at the time of impact.

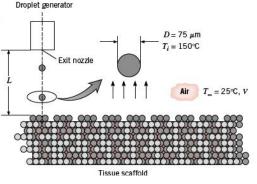


Consider conditions for which droplets with a diameter, velocity, and initial temperature of  $D = 500 \ \mu m$ ,  $V = 3 \ m/s$ , and  $T_i = 1100 \ K$ , respectively, traverse a stagnant layer of atmospheric helium that is at a temperature of  $T_{\infty} = 300 \ K$ . What is the maximum allowable thickness of the helium layer needed to ensure that the temperature of droplets impacting the substrate is greater than or equal to the melting point of aluminum ( $T_f \ge T_{mp} = 933 \ K$ )? Properties of the molten aluminum may be approximated as  $\rho = 2500 \ \text{kg}/\text{m}^3$ ,  $c = 1200 \ \text{J/kg} \cdot \text{K}$ , and  $k = 200 \ \text{W/m} \cdot \text{K}$ .

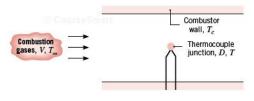
7.77 Tissue engineering involves the development of biological substitutes that restore or improve tissue function. Once manufactured, engineered organs can be implanted and grow within the patient, obviating chronic shortages of natural organs that arise when traditional organ transplant procedures are used. Artificial organ manufacture involves two major steps. First, a porous *scaffold* is fabricated with a specific pore size and pore distribution, as well as overall shape and size. Second, the top surface of the scaffold is seeded with human cells that grow into the pores of the scaffold. The scaffold material is biodegradable and is eventually replaced with healthy tissue. The artificial organ is then ready to be implanted in the patient.

The complex pore shapes, small pore sizes, and unusual organ shapes preclude use of traditional manufacturing methods to fabricate the scaffolds. A method that has been used with success is a *solid freeform fabrication* technique whereby small spherical drops are directed to a substrate. The drops are initially molten and solidify when they impact the room-temperature substrate. By controlling the location of the droplet deposition, complex scaffolds can be built up, one drop at a time. A device similar to that of Problem 7.71 is used to generate uniform, 75- $\mu$ m-diameter drops at an initial temperature of  $T_i = 150^{\circ}$ C. The particles are sent through quiescent air at  $T_{\infty} = 25^{\circ}$ C. The droplet properties are  $\rho = 2200 \text{ kg/m}^3$ ,  $c = 700 \text{ J/kg} \cdot \text{K}$ .

- (a) It is desirable for the droplets to exit the nozzle at their terminal velocity. Determine the terminal velocity of the drops.
- (b) It is desirable for the droplets to impact the structure at a temperature of T<sub>2</sub> = 120°C. What is the required distance between the exit nozzle and the structure, L?



7.78 A spherical thermocouple junction 1.0 mm in diameter is inserted in a combustion chamber to measure the temperature  $T_{\infty}$  of the products of combustion. The hot gases have a velocity of V = 5 m/s.



- (a) If the thermocouple is at room temperature, T<sub>ρ</sub> when it is inserted in the chamber, estimate the time required for the temperature difference, T<sub>∞</sub> - T, to reach 2% of the initial temperature difference, T<sub>∞</sub> -T<sub>ρ</sub>. Neglect radiation and conduction through the leads. Properties of the thermocouple junction are approximated as k = 100 W/m · K, c = 385 J/kg · K, and ρ = 8920 kg/m<sup>3</sup>, while those of the combustion gases may be approximated as k = 0.05 W/m · K, ν = 50 × 10<sup>-6</sup> m<sup>2</sup>/s, and Pr = 0.69.
- (b) If the thermocouple junction has an emissivity of 0.5 and the cooled walls of the combustor are at

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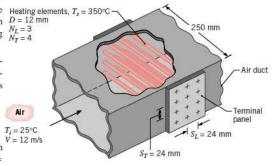
Chapter 7 
External Flow

- (a) The stress test begins with the components at ambient temperature ( $T_i = 20^{\circ}$ C) and proceeds with heating by the fluid at  $T_{\infty} = 80^{\circ}$ C. If the fluid velocity is V = 0.2 m/s, estimate the ratio of the time constant of the chip to that of a solder ball. Which component responds more rapidly to the heating  $N_L = 3$  $N_T = 4$
- (b) The thermal stress acting on the solder joint is proportional to the chip-to-solder temperature difference. What is this temperature difference 0.25 s after the start of heating?

## **Tube Banks**

- 7.83 Repeat Example 7.7 for a more compact tube bank in which the longitudinal and transverse pitches are  $S_L = S_T = 20.5$  mm. All other conditions remain the same.
- **7.84** A preheater involves the use of condensing steam at 100°C on the inside of a bank of tubes to heat air that enters at 1 atm and 25°C. The air moves at 5 m/s in cross flow over the tubes. Each tube is 1 m long and has an outside diameter of 10 mm. The bank consists of 196 tubes in a square, aligned array for which  $S_T = S_L = 15$  mm. What is the total rate of heat transfer to the air? What is the pressure drop associated with the airflow?
- **7.85** Consider the in-line tube bank of Problem 7.84 (D = 10 mm, L = 1 m, and  $S_T = S_L = 15$  mm), with condensing steam used to heat atmospheric air entering the tube bank at  $T_i = 25^{\circ}$ C and V = 5 m/s. In this case, however, the desired outlet temperature, not the number of tube rows, is known. What is the minimum value of  $N_L$  needed to achieve an outlet temperature of  $T_o \ge 75^{\circ}$ C? What is the corresponding pressure drop across the tube bank?
- **7.86** A tube bank uses an aligned arrangement of 10-mmdiameter tubes with  $S_T = S_L = 20$  mm. There are 10 rows of tubes with 50 tubes in each row. Consider an application for which cold water flows through the tubes, maintaining the outer surface temperature at  $27^{\circ}$ C, while flue gases at  $427^{\circ}$ C and a velocity of 5 m/s are in cross flow over the tubes. The properties of the flue gas may be approximated as those of atmospheric air at  $427^{\circ}$ C. What is the total rate of heat transfer per unit length of the tubes in the bank?
- **7.87** An air duct heater consists of an aligned array of electrical heating elements in which the longitudinal and transverse pitches are  $S_L = S_T = 24$  mm. There are 3 rows of elements in the flow direction ( $N_L = 3$ ) and 4 elements per row ( $N_T = 4$ ). Atmospheric air with an upstream velocity of 12 m/s and a temperature of 25°C moves in cross flow over the elements, which have a diameter of

12 mm, a length of 250 mm, and are maintained at a surface temperature of  $350^{\circ}\text{C}.$ 



- (a) Determine the total heat transfer to the air and the temperature of the air leaving the duct heater.
- (b) Determine the pressure drop across the element bank and the fan power requirement.
- (c) Compare the average convection coefficient obtained in your analysis with the value for an isolated (single) element. Explain the difference between the results.
- (d) What effect would increasing the longitudinal and transverse pitches to 30 mm have on the exit temperature of the air, the total heat rate, and the pressure drop?
- **7.88** A tube bank uses an aligned arrangement of 30-mmdiameter tubes with  $S_T = S_L = 60$  mm and a tube length of 1 m. There are 10 tube rows in the flow direction  $(N_L = 10)$  and 7 tubes per row  $(N_T = 7)$ . Air with upstream conditions of  $T_{\infty} = 27^{\circ}$ C and V = 15 m/s is in cross flow over the tubes, while a tube wall temperature of 100°C is maintained by steam condensation inside the tubes. Determine the temperature of air leaving the tube bank, the pressure drop across the bank, and the fan power requirement.
- **7.89** Electrical components mounted to each of two isothermal plates are cooled by passing atmospheric air between the plates, and an in-line array of aluminum pin fins is used to enhance heat transfer to the air.
  - The pins are of diameter D = 2 mm, length L = 100 mm, and thermal conductivity k = 240 W/m · K. The longitudinal and transverse pitches are  $S_L = S_T = 4$  mm, with a square array of 625 pins ( $N_T = N_L = 25$ ) mounted to square plates that are each of width W = 100 mm on a side. Air enters the pin array with a velocity of 10 m/s and a temperature of 300 K.
  - (a) Evaluating air properties at 300 K, estimate the average convection coefficient for the array of pin fins.